

Advanced Fluid Dynamics : Sheet 2

1. $\underline{u} = (u, v)$ $u = \frac{\partial \psi}{\partial y}$ $v = -\frac{\partial \psi}{\partial x}$

(a) Streamlines, $\frac{dx}{dt} = u$, $\frac{dy}{dt} = v$

(b) $\frac{d\psi}{dt} = \frac{\partial \psi}{\partial x} \frac{dx}{dt} + \frac{\partial \psi}{\partial y} \frac{dy}{dt} = -v u + u v = 0$

Streamlines are given by $\psi = \text{constant}$.

(b) $u = \alpha x - \omega y = \frac{\partial \psi}{\partial y} \Rightarrow \psi = \alpha x y - \frac{1}{2} \omega y^2 + f(x)$
 $v = -\alpha y + \omega x = -\frac{\partial \psi}{\partial x} \Rightarrow \psi = \alpha x y - \frac{1}{2} \omega x^2 + g(y)$

Hence $\psi = \alpha x y - \frac{1}{2} \omega (x^2 + y^2)$ [upto additive constant]

$\psi = \text{constant} \Rightarrow x^2 + y^2 - 2\frac{\alpha}{\omega} x y = \text{const}$

$(x+y)^2 + \lambda(x-y)^2 = (\lambda+1)(x^2+y^2) + 2xy(1-\lambda)$

$x^2 + y^2 - 2\frac{\alpha}{\omega} x y = \frac{1}{\lambda+1} \left((x+y)^2 + \lambda(x-y)^2 \right)$ if $\frac{1-\lambda}{1+\lambda} = -\frac{\alpha}{\omega}$

Hence $\psi = c = \frac{1}{\left(\frac{-2\omega}{\alpha-\omega}\right)} \left((x+y)^2 - \frac{(\alpha+\omega)}{(\alpha-\omega)} (x-y)^2 \right)$

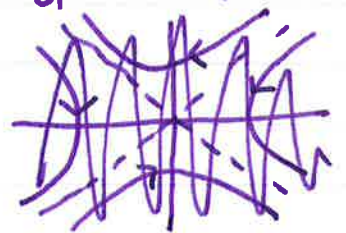
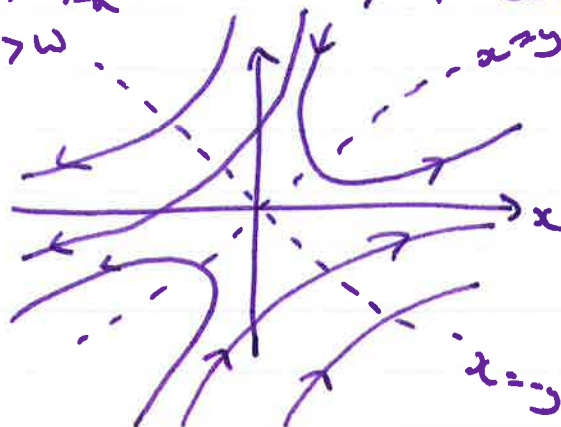
$\Rightarrow \lambda \left(\frac{\alpha}{\omega} - 1 \right) = - \left(\frac{\alpha}{\omega} + 1 \right)$

$\lambda = -\frac{(\alpha+\omega)}{\alpha-\omega}$

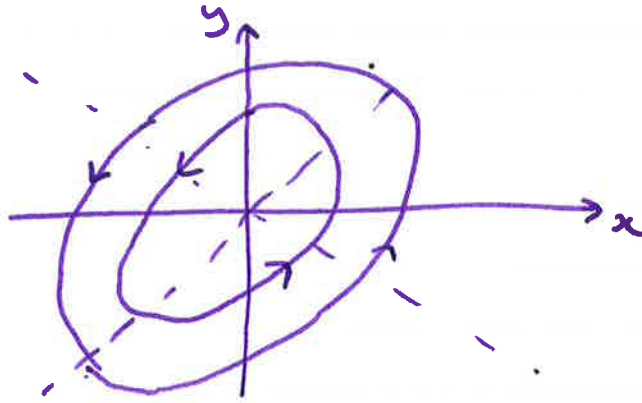
$\lambda + 1 = -\frac{2\omega}{\alpha-\omega}$

So if $\alpha > \omega \Rightarrow \lambda < 0 \Rightarrow \psi = \text{const}$ gives hyperbolae.

i.e. $|\alpha| > \omega$



If $\omega > \frac{|x|}{R} \Rightarrow \lambda > 0 \Rightarrow \psi = \text{const}$ gives ellipses



(c) Navier-Stokes equations (already $\frac{\partial}{\partial t} = 0$)

$$\underline{u} \cdot \nabla \underline{u} = -\frac{1}{\rho} \nabla p + \nu \nabla^2 \underline{u}$$

$$\frac{1}{\rho} \frac{\partial p}{\partial x} = \nu \left(\frac{\partial^2 u}{\partial x^2} + \frac{\partial^2 u}{\partial y^2} \right) - u \frac{\partial u}{\partial x} - v \frac{\partial u}{\partial y} = -(\alpha x - \omega y)\alpha - (-\alpha y + \omega x)\omega$$

$$\frac{1}{\rho} \frac{\partial p}{\partial y} = \nu \left(\frac{\partial^2 v}{\partial x^2} + \frac{\partial^2 v}{\partial y^2} \right) - u \frac{\partial v}{\partial x} - v \frac{\partial v}{\partial y} = -(\alpha x - \omega y)\omega - (-\alpha y + \omega x)\alpha$$

$$\Rightarrow \frac{1}{\rho} \frac{\partial p}{\partial x} = (\omega^2 - \alpha^2)x$$

$$\text{and } \frac{1}{\rho} \frac{\partial p}{\partial y} = (\omega^2 - \alpha^2)y$$

pressure
(to which additive constant)

$$p = \frac{1}{2}\rho(\omega^2 - \alpha^2)(x^2 + y^2)$$

(d) $\omega^2 > \alpha^2 \Rightarrow p$ increases away from $x=y=0$

$\Rightarrow p$ is minimum at origin.

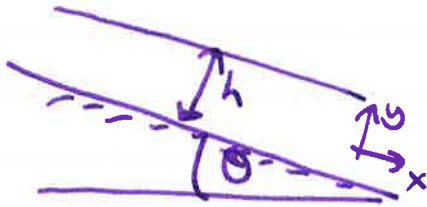
$\omega^2 < \alpha^2 \Rightarrow p$ decreases away from $x=y=0$

$\Rightarrow p$ is maximum at origin.

$\omega^2 > \alpha^2$: to maintain "circular" motion about the origin, fluid elements must be accelerated inwards \Rightarrow inward pressure gradient

$\omega^2 < \alpha^2$: fluid elements are "repelled" from the origin (stagnation point) thus must have locally maximum pressure at the origin.

2.



$$\underline{u} = u(y) \hat{x}$$

$$\nabla \cdot \underline{u} = 0 \quad (\text{automatically})$$

$$\text{Navier Stokes: } \underline{u} \cdot \nabla \underline{u} = -\frac{1}{\rho} \nabla p + \nu \nabla^2 \underline{u} + \underline{g}$$

$$0 = -\frac{1}{\rho} \frac{dp}{dx} + \nu \frac{d^2 u}{dy^2} + g \sin \theta$$

$$0 = -\frac{1}{\rho} \frac{dp}{dy} + 0 = g \cos \theta$$

$$\text{Thus pressure } p = \rho g \cos \theta (h-y) + p_{\text{atm.}} \quad \text{where } p_{\text{atm.}} = \text{atmospheric pressure.}$$

$$\text{Streamwise pressure gradient } \frac{dp}{dx} = 0$$

$$\Rightarrow 0 = \nu \frac{d^2 u}{dy^2} + g \sin \theta$$

$$\Rightarrow u(y) = -\frac{g \sin \theta}{2\nu} \frac{y^2}{2} + Ay + B \quad A, B \text{ constants}$$

$$\text{At } y=0, \text{ no-slip condition } u(y)=0 \Rightarrow B=0$$

$$\text{At } y=h, \text{ free-surface } \Rightarrow \frac{du}{dy} = 0 \Rightarrow -\frac{g \sin \theta}{\nu} h + A = 0$$

$$\Rightarrow u(y) = \frac{g \sin \theta}{2\nu} \left(hy - \frac{y^2}{2} \right)$$

$$\begin{aligned} \text{Volume flux per unit width } q &= \int_0^h u dy = \frac{g \sin \theta}{2\nu} \left[\frac{hy^2}{2} - \frac{y^3}{6} \right]_0^h \\ &= \frac{\rho g \sin \theta}{\mu} \frac{h^3}{3} \end{aligned}$$

3. For stationary boundaries, viscous dissipation $D = 2\mu \int_V e_{ij} e_{ij} dV$

where $e_{ij} = \frac{1}{2} (\sigma_i u_j + \sigma_j u_i)$

$$\begin{aligned} e_{ij} e_{ij} &= \frac{1}{4} (\sigma_i u_j + \sigma_j u_i) (\sigma_i u_j + \sigma_j u_i) \\ &= \frac{1}{4} (\sigma_i u_j - \sigma_j u_i) (\sigma_i u_j - \sigma_j u_i) + \sigma_j u_i \sigma_i u_j \\ &= \Omega_{ij} \Omega_{ij} + \sigma_i [\sigma_j u_i u_j] \quad \text{since } \nabla \cdot \underline{u} = 0 \end{aligned}$$

$$\begin{aligned} \int_V 2\mu e_{ij} e_{ij} dV &= \int_V 2\mu \Omega_{ij} \Omega_{ij} dV + \int_V 2\mu \sigma_i (\sigma_j u_i u_j) dV \\ &= 2\mu \int_V \Omega_{ij} \Omega_{ij} dV + \int_S 2\mu n_i \sigma_j u_i u_j dS \\ &\quad \text{(by divergence theorem)} \end{aligned}$$

but $\int_S 2\mu n_i \sigma_j u_i u_j dS = \int_S 2\mu (\underline{u} \cdot \nabla) (\underline{u} \cdot \underline{n}) dS$
 (but $\underline{u} = 0$ on S) $= 0$

$$\Omega_{ij} = \frac{1}{2} \epsilon_{ijk} \omega_k \quad \epsilon_{ijl} \Omega_{ij} = \frac{1}{2} \epsilon_{ijl} \epsilon_{ijk} \omega_k = \frac{1}{2} (3\delta_{lk} - \delta_{lk}) \omega_k = \frac{2\omega_l}{2} = \omega_l$$

$$\begin{aligned} \text{so } \Omega_{ij} \Omega_{ij} &= \frac{1}{4} \epsilon_{ijk} \omega_k \epsilon_{ijp} \omega_p \\ &= \frac{1}{4} (\delta_{jp} \delta_{kp} - \delta_{jp} \delta_{kp}) \omega_p \omega_k \\ &= \frac{1}{4} (3 - 1) |\underline{\omega}|^2 = \frac{1}{2} |\underline{\omega}|^2 \end{aligned}$$

Thus $D = \int_V 2\mu \cdot \frac{1}{2} |\underline{\omega}|^2 dV$

For irrotational flows $\underline{\omega} = 0 \Rightarrow$ dissipation $D = 0$.

* Velocity field $\underline{u} = w(r)\hat{z}$ $\frac{dp}{dz} = -G$

$\nabla \cdot \underline{u} = 0$ automatically, Navier-Stokes $\frac{1}{r} \frac{d}{dr} (r \frac{dw}{dr}) = -\frac{G}{\mu}$

$\Rightarrow r \frac{dw}{dr} = -\frac{G}{\mu} \frac{r^2}{2} + A$

$\Rightarrow w = B + A \log r - \frac{G}{4\mu} r^2$

No-slip conditions

$w(a) = 0 \quad 0 = B + A \log a - \frac{G}{4\mu} a^2 \quad \text{--- (1)}$

$w(b) = 0 \quad 0 = B + A \log b - \frac{G}{4\mu} b^2 \quad \text{--- (2)}$

Between (1) and (2) $A \log \frac{a}{b} = \frac{G}{4\mu} (a^2 - b^2)$

and $B = \frac{G}{4\mu} a^2 - \frac{G}{4\mu} \frac{(a^2 - b^2) \log a}{\log a/b}$

Here $w(r) = \frac{G}{4\mu} (a^2 - r^2) + \frac{G}{4\mu} \frac{(a^2 - b^2) \log r/a}{\log a/b}$

Volume flux $Q = 2\pi \int_b^a r w dr = \frac{2\pi G}{4\mu} \left[\frac{a^2 r^2}{2} - \frac{r^4}{4} \right]_b^a + \frac{2\pi G}{4\mu} \frac{(a^2 - b^2)}{\log a/b} \int_b^a r \log \frac{r}{a} dr$

now $\int_b^a r \log \frac{r}{a} dr = \left[\frac{r^2}{2} \log \frac{r}{a} \right]_b^a - \int_b^a \frac{r}{2} dr$
 $= -\frac{1}{2} b^2 \log \frac{b}{a} - \frac{1}{4} (a^2 - b^2)$

Here $Q = \frac{\pi G}{2\mu} \left(\frac{a^4}{4} - \frac{a^2 b^2}{2} + \frac{b^4}{4} \right) + \frac{\pi G}{2\mu} \frac{(a^2 - b^2)}{\log a/b} \left(-\frac{1}{2} b^2 \log \frac{b}{a} - \frac{1}{4} (a^2 - b^2) \right)$

$= \frac{\pi G}{8\mu} (a^4 - b^4) + \frac{\pi G}{8\mu} \frac{(a^2 - b^2)^2}{\log a/b}$

(i) $b = \epsilon a \quad Q = \frac{\pi G a^4}{8\mu} \left[1 - \epsilon^4 + \frac{(1 - \epsilon^2)^2}{\log 1/\epsilon} \right]$
 $= \frac{\pi G a^4}{8\mu} \left(1 - \frac{1}{\log 1/\epsilon} + \dots \dots \right)$

(ii) $b = (1 - \epsilon) a \quad Q = \frac{\pi G a^4}{8\mu} \left[1 - (1 - \epsilon)^4 - \frac{(1 - (1 - \epsilon)^2)^2}{\log 1/\epsilon} \right]$

$$= \frac{\pi G a^4}{8\mu} \left[1 - (1 - 4\varepsilon + 6\varepsilon^2 - 4\varepsilon^3 + \dots) + \frac{(2\varepsilon - \varepsilon^2)^2}{\log(1-\varepsilon)} \right]$$

$$\log(1-\varepsilon) = -\varepsilon - \frac{1}{2}\varepsilon^2 - \frac{1}{3}\varepsilon^3 + \dots$$

$$\begin{aligned} \frac{(2\varepsilon - \varepsilon^2)^2}{\log(1-\varepsilon)} &= \frac{\varepsilon^2(2-\varepsilon)^2}{-\varepsilon - \frac{1}{2}\varepsilon^2 - \frac{1}{3}\varepsilon^3} = \varepsilon(2-\varepsilon)^2 \left(-1 + \frac{1}{2}\varepsilon + \frac{1}{12}\varepsilon^2 + \dots \right) \\ &= -4\varepsilon + 6\varepsilon^2 - \frac{8}{3}\varepsilon^3 + \dots \end{aligned}$$

$$\begin{aligned} \text{Hence } Q &= \frac{\pi G a^4}{8\mu} \left[4\varepsilon - 6\varepsilon^2 + 4\varepsilon^3 - 4\varepsilon + 6\varepsilon^2 - \frac{8}{3}\varepsilon^3 + \dots \right] \\ &= \frac{\pi G a^4}{6\mu} \varepsilon^3 + \dots \end{aligned}$$

This result could have been anticipated

$$Q = 2\pi a \cdot \frac{G(\varepsilon a)^3}{12\mu} \quad \text{and} \quad \frac{G(\varepsilon a)^3}{12\mu} \text{ is flow flux in channel of width } \varepsilon a.$$